

11-17-00

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jc957 U.S. PTO  
11/16/00

CERTIFICATE OF EXPRESS MAIL

NUMBER EL521293419US

DATE OF DEPOSIT November 16, 2000

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jc715 U.S. PTO  
09/714469  
00/91/11

**PATENT**

**IN THE UNITED STATES PATENT AND TRADEMARK OFFICE**

**Atty. Dkt. No.: 11899.0189.DVUS00  
(MOBT:189--2)**

**Prior Application Examiner:  
T. Yoon**

**BOX PATENT APPLICATION**  
Assistant Commissioner for Patents  
Washington, D.C. 20231

**Classification Designation:  
524**

**Prior Group Art Unit: 1714**

**REQUEST FOR FILING DIVISIONAL APPLICATION  
UNDER 37 C.F.R. § 1.53(b)**

This is a request for filing a divisional application under Rule 53(b) (37 C.F.R. § 1.53(b)) of co-pending prior application Serial No. 09/179,780 filed October 27, 1998, entitled "Polymer Blends Containing Polyhydroxyalkanoates and Compositions With Good Retention of Elongation."

- ☒ 1. Enclosed is a copy of the prior application Serial No. 09/179,780 as originally filed, including specification, claims and declaration. The undersigned hereby verifies that the attached papers are a true copy of the prior application as originally filed and identified above, that no amendments (if any) referred to in the declaration filed to complete the prior application introduced new matter therein, and further that this statement was made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment or

both, under Section 1001 of Title 18 of the United States Code, and that such willful false statement may jeopardize the validity of the application or any patent issuing thereon.

(a) ☒ The inventorship is the same as prior Application Serial No. 09/179,780.

(b) ☐ Deletion of inventor(s). Signed statement attached deleting inventor(s) named in the prior application, see 37 C.F.R. § 1.63(d)(2) and 1.33(b).

(c) ☐ Priority of foreign patent application number \_\_\_\_\_, filed \_\_\_\_\_ in \_\_\_\_\_ is claimed under 35 U.S.C. § 119(a)-(e). The certified copy:

☐ is enclosed.

☐ has been filed in the prior Application Serial No. \_\_\_\_\_.

☒ 2. The Assistant Commissioner is requested to grant Applicants a filing date in accordance with Rule 1.53, and supply Applicants with a Notice of Missing Parts in due course, in accordance with the provisions of Rule 1.53(f).

☒ 3. The Assistant Commissioner is authorized to charge the deposit account of Howrey Simony Arnold & White, LLP, No. 01-2508/118990189DVUS00 the filing fee as calculated below and the fee for any new claims added in the Preliminary Amendment referred to in Part No. 9 below.

CLAIMS AS FILED IN THE PRIOR APPLICATION  
LESS CLAIMS CANCELED BELOW

FOR	NUMBER FILED	NUMBER EXTRA	RATE	FEE
Basic Fee -----				710.00
Total Claims	8 - 20 =	0 X	\$18.00 =	0.00
Independent Claims	4 - 3 =	1 X	\$80.00 =	80.00
Multiple Dependent Claim(s) -----				\$-0-
<b>TOTAL FILING FEES:</b>				<b>790.00</b>

- ☐ 4. Applicant is entitled to Small Entity Status for this application.
- ☐ (a) A small entity statement is enclosed.
- ☐ (b) A small entity statement was filed in the prior nonprovisional application and such status is still proper and desired.
- ☐ (c) Small entity status is no longer claimed.
- ☒ 5. The Assistant Commissioner is authorized to further charge Deposit Account No. 01-2508/118990189DVUS00 for any additional fees under 37 C.F.R. §§ 1.16 to 1.21 that should be required for any reason relating to the enclosed materials.
- ☒ 6. Enclosed is a copy of the current Power of Attorney in the prior application.
- ☒ 7. Address all future communications to:
- Patricia A. Kammerer  
HOWREY SIMON ARNOLD & WHITE, LLP  
750 Bering Drive  
Houston, Texas 77057-2198  
(713) 787-1400
- ☒ 8. The prior application is presently assigned to Monsanto Company.

- ☒ 9. Enclosed is a preliminary amendment. Any additional fees incurred by this amendment are included at No. 3 above and said fee has been calculated after calculation of claims and after amendment of claims by the preliminary amendment.
- ☒ 10. Cancel in this application claims 1-41 of the prior application before calculating the filing fee. (At least one original independent claim must be retained).
- ☒ 11. Amend the specification by inserting before the first line the sentence: --This is a divisional of co-pending application Serial No. 09/179,780 filed October 27, 1998--.
- ☐ 12. Enclosed are formal drawings.
- ☒ 13. An Information Disclosure Statement (IDS) is enclosed.
- ☒ (a) PTO-1449.
- ☐ (b) Copies of IDS citations.
- ☐ 14. Transfer the sequence information, including the computer readable form previously submitted in the parent application, Serial No.                      filed                      , for use in this application. Under 37 C.F.R. § 1.821(e), Applicant states that the paper copy of the sequence listing in this application is identical to the computer readable copy in parent application Serial No.                      filed                      . Under 37 C.F.R. § 1.821(f), Applicant also states that the information recorded in computer readable form is identical to the written sequence listing.

- ☐ 15. Other:
- ☒ 16. Return Receipt Postcard.

Respectfully submitted,



Patricia A. Kammerer

Reg. No. 29,775

Attorney for Assignee

MONSANTO COMPANY

HOWREY SIMON ARNOLD & WHITE, LLP  
750 Bering Drive  
Houston, TX 77057-2198  
(713) 787-1400

Date: Nov 15, 2000

CERTIFICATE OF EXPRESS MAIL

NUMBER EL521293419US

DATE OF DEPOSIT November 16, 2000

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Signature

**PATENT**

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

*In re* Application of:

Jawed Asrar

Jean R. Pierre

Group Art Unit: Unknown

Examiner: Unknown

Serial No.: Unknown

Atty. Dkt. No.: 11899.1089.DVUS00  
MOBT:189--2

Filed: Concurrently herewith

For: POLYMER BLENDS CONTAINING  
POLYHYDROXYALKANOATES AND  
COMPOSITIONS WITH GOOD  
RETENTION OF ELONGATION

**PRELIMINARY AMENDMENT**

Assistant Commissioner for Patents  
Washington, D.C. 20231

Dear Sir:

Please amend this application as follows:

**In The Specification**

At page 2, line 1, insert the following:

--This is a divisional of co-pending application Serial No. 09/179,780, filed October 27,  
1998.--

### In the Claims

Please cancel claims 1-41, without prejudice and amend claims 44 and 45 as follows:

44. The composition of claim 42 wherein the nucleant is present at levels from 0.1 to 20 wt% of the [blend] composition.
45. The composition of claim 42 wherein the nucleant is present at levels from 1 to 10 wt% of the [blend] composition.

### REMARKS

Claims 1-41 were prosecuted in the parent case, application Serial No. 09/179,780 and thus have been canceled from this divisional application. The parent application was allowed on September 13, 2000 but has not yet issued.

The active claims in this case are claims 42-49.

It is believed that no fee is due; however, should any fees under 37 C.F.R. §§ 1.16 to 1.21 be required for any reason relating to the enclosed materials, the Assistant Commissioner is authorized to deduct said fees from Howrey Simon Arnold & White Deposit Account No. 01-2508/11899.0189.DVUS00/KAM.

Respectfully submitted,



Patricia A. Kammerer

Reg. No. 29,775

Attorney for Assignee

MONSANTO COMPANY

HOWREY SIMON ARNOLD & WHITE, LLP  
750 Bering Drive  
Houston, TX 77057-2198  
(713) 787-1400

Date: Nov 15, 2000

**APPLICATION FOR UNITED STATES LETTERS PATENT**

**for**

**POLYMER BLENDS CONTAINING POLYHYDROXYALKANOATES AND  
COMPOSITIONS WITH GOOD RETENTION OF ELONGATION**

**by**

**Jawed Asrar**

**Jean R. Pierre**

**EXPRESS MAILING NUMBER:  
DATE OF DEPOSIT:**

**EI371155817US  
October 27, 1998**



This application is based on United States Provisional Application No. 60/063,852, filed October 31, 1997.

### **BACKGROUND OF THE INVENTION**

5           The present invention relates generally to biodegradable polymers. More particularly, it concerns biodegradable polymer blends containing oligomeric esters and use of such blends in the production of shaped polymeric objects having improved properties which do not diminish over time.

10           There has been considerable interest in recent years in the use of biodegradable polymers to address concerns over plastic waste accumulation. The potential worldwide market for biodegradable polymers is enormous (> 10B lbs/yr). Some of the markets and applications most amenable to the use of such biopolymers range from single use applications, which can include packaging, personal hygiene, garbage bags, and others where the biopolymers become soiled and  
15           are ideally suited for biodegradation through composting, to markets and applications in which the biopolymers can be recovered as clean materials, such as garment bags, shopping bags, grocery bags, etc. and are suitable for recycling, as well as composting, or biodegradation in landfills.

20           Polyhydroxyalkanoate (PHA) biopolymers are thermoplastic polyesters, many of which can be produced by microorganisms in response to nutrient limitation. The commercial potential for PHA's spans many industries, and is derived primarily from certain advantageous properties which distinguish PHA polymers from petrochemical-derived polymers, namely excellent biodegradability and natural renewability.

25           Widespread use and acceptance of PHA's, however, has been hindered by certain undesirable chemical and physical properties of these polymers. For example, PHA's are among the most thermosensitive of all commercially available polymers. As such, the rate of polymer

degradation, as measured by a decrease in molecular weight, increases sharply with increasing temperatures in the range typically required for conventional melt-processing of PHA's into end-products such as films, coatings, fibers etc. An additional limitation of the potential utility of PHA polymers relates to the observation that some polymer characteristics, for example ductility, elongation, impact resistance, and flexibility, diminish over time. This rapid "aging" of certain PHA-derived products is unacceptable for most commercial applications. Thus, the success of PHA as a viable alternative to both petrochemical-derived polymers and to non-PHA biodegradable polymers, will depend upon novel approaches to overcome the unique difficulties associated with PHA polymers and with products derived therefrom.

The blending of two or more polymers has become an increasingly important approach for improving the cost performance of commercial plastics. For example, blending may be used to reduce the cost of an expensive engineering thermoplastic, to improve the processability of a high-temperature or heat sensitive thermoplastic, to improve impact resistance, etc. Therefore, blending is one approach which has the potential to provide new classes of biodegradable PHA-containing polymers having unique and improved properties. In this way, it may be possible to overcome the limitations of PHA compositions that have limited their widespread industrial utilization while retaining their desirable features. Unfortunately, many polymers are immiscible when blended, and result in undesirable phase separation during processing. Generally, such blends of incompatible or thermodynamically immiscible polymers exhibit poor mechanical properties and processing difficulties.

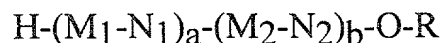
Compatibilizing compounds have been identified and developed for numerous polymer systems. These compounds can reduce interfacial tension and thereby promote miscibility of otherwise poorly miscible polymers. The availability of compatibilizers provides an effective means by which polymeric compositions can be produced. However, with PHAs, very little has been achieved in this regard, and there is a need for the identification of compounds providing

effective compatibilization of blends containing different PHA polymers or blends containing PHA and non-PHA polymers.

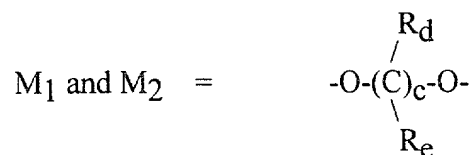
### SUMMARY OF THE INVENTION

In accordance with one aspect of the present invention, there are provided polymer compositions comprising a first biodegradable polymer comprising a polyhydroxyalkanoate (PHA), a second biodegradable polymer different from said first polymer, and one or more oligomeric esters. It has been found that the presence of oligomeric esters as described herein provide advantageous properties to blends of two or more biodegradable polymers. As a result, blends containing the oligomeric esters exhibit ductility, impact strength and aging characteristics improved to an unexpected and unpredictable extent.

Most oligomeric esters useful in the blend compositions of this invention can be represented by following structural formula:



where:



X is C<sub>6</sub>H<sub>4</sub> or (CH<sub>2</sub>)<sub>f</sub>

a and b are independently 0 or an integer from 1 to 200;

c and f are independently integers from 1 to 30;

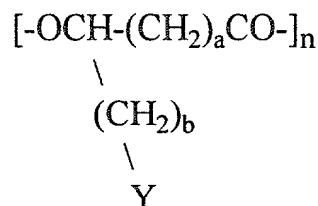
R is H or C<sub>1</sub>-C<sub>12</sub> alkyl or branched alkyl; and

R<sub>d</sub> and R<sub>e</sub> are H, or C<sub>1</sub>-C<sub>12</sub> alkyl or branched alkyl and can vary independently with each (C)<sub>c</sub>.

In a preferred class of oligomeric esters, f is 2 to 10. Most preferably, the compounds are oligomeric adipic esters, i.e., f is 4.

The oligomeric ester generally will be present in the blend at a level from 1 to 20 wt.%, preferably 2 to 15 wt.% of the blend. The molecular weights of the oligomeric esters are typically in the range of 200 to 20,000, preferably 500 to 15,000, and most preferably from about 1500 to 7500.

At least one of the polymers in the blend is a PHA, preferably having the structural formula:



where a= 1-4, b=0-15, Y is H, and n is an integer. In a most preferred composition, one of the polymers in the blend is polyhydroxybutyrate (PHB) or polyhydroxybutyrate-co-valerate (PHBV).

A second polymer in the blend can be a PHA structurally distinct from the first PHA, or can be a non-PHA biodegradable polymer. The non-PHAs can be, for example, aliphatic polyesters or copolyesters derived from aliphatic dicarboxylic acids or anhydrides, aliphatic dicarboxylic acid chlorides, aliphatic dicarboxylic acid esters, and aliphatic diols or epoxides; polyurethanes made from said polyesters and copolyesters by reaction with a diisocyanate; aliphatic polycarbonates; polyanhydrides; polyester amides; polyester carbonates; polyester ethers; or polyether carbonates. Preferred non-PHA polymers for use in the invention include aliphatic polyesters and copolyesters, and polyester urethanes. More preferred non-PHA polymers include polycaprolactone (PCL, e.g. Tone 187P PCL, Union Carbide) and polybutylenesuccinate-adipate (PBSUA, e.g. Bionolle 3001 PBSUA, Showa High Polymer Co.).

In a most preferred composition of this invention, blends are provided which comprise a PHA, polycaprolactone, and an oligomeric ester. The oligomeric ester is preferably an oligomeric adipic ester, such as poly(1,3-butylene glycol-co-1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\*S409A; Mw = 3700, available from Solutia Inc.), poly(neopentyl glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\*S433; Mw = 3500, available from Solutia Inc.), poly(1,3-butylene glycol adipic acid) unterminated (Santicizer\*S430; Mw = 2500, available from Solutia Inc.), poly(1,3-butylene glycol adipic acid) unterminated (Santicizer\*S421; Mw = 1250, available from Solutia Inc.), poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol (Santicizer\*S438; Mw = 1900, available from Solutia Inc.), poly(neopentyl glycol adipic acid) terminated with 2-ethylhexanol (Santicizer \*S435; Mw = 2500; available from Solutia Inc.), poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol (Santicizer \*431; Mw = 1200; available from Solutia Inc.), poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2 ethylhexanol (Santicizer \*S4212; Mw = 950; available from Solutia Inc.), poly (1,3-butylene glycol adipic acid) terminated with mixed fatty acids (Santicizer \*S405; Mw = 2000; available from Solutia Inc.), poly(1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\* S436; Mw = 3500; available from Solutia Inc.), poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer \*S449; Mw = 3700; available from Solutia Inc.), poly(1,4-butylene glycol adipic acid), or poly(1,4-butylene glycol-co-ethylene glycol adipic acid).

In accordance with another aspect of this invention, there is provided a method of producing a shaped polymeric object comprising melting a composition comprising a polyhydroxyalkanoate (PHA), a second biodegradable polymer different from the first polymer, and one or more oligomeric esters, and producing a shaped object therefrom, for example by extrusion, molding, coating, spinning or calendaring operations.

5 In accordance with yet another aspect of the present invention, there are provided polymer compositions comprising a first biodegradable polymer comprising a poly-3-hydroxybutyrate-co-4-hydroxybutyrate (P3HB4HB) and a nucleant. It has been found that such compositions exhibit ductility, impact strength and aging characteristics improved to an unexpected and unpredictable extent.

10 P3HB4HB is a copolymer of 3-hydroxybutyrate (3HB) and 4-hydroxybutyrate (4HB), wherein the 3HB repeat unit has the structural formula above wherein  $Y=H$ ,  $b=1$ ,  $a=1$ , and  $n=1$ , and wherein the 4HB repeat unit has the structural formula above wherein  $Y=H$ ,  $b=0$ ,  $a=2$ , and  $n=1$ . The nucleant can be any nucleant known to be effective in nucleating PHAs. A preferred nucleant is boron nitride.

15 In accordance with another aspect of this invention, there is provided a method of producing a shaped polymeric object comprising melting a composition comprising poly-3-hydroxybutyrate-co-4-hydroxybutyrate (P3HB4HB) and a nucleant, and producing a shaped object therefrom, for example by extrusion, molding, coating, spinning or calendaring operations.

### DESCRIPTION OF ILLUSTRATIVE EMBODIMENTS

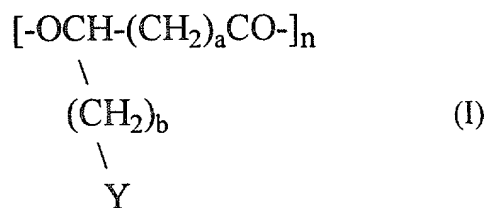
20 The embodiments of the present invention relate broadly to compositions for use in the production of PHA-containing materials having wide-ranging properties that can serve to increase the versatility and performance of PHAs for various processing techniques without sacrificing biodegradability.

25 "Polymer blend" as used herein refers to a composition which comprises two or more structurally distinct biodegradable polymers. A first polymer in the blend is preferably a PHA. A second polymer in the blend can also be a PHA provided it is structurally distinct from the first polymer. Alternatively, the second polymer can be a biodegradable non-PHA polymer. Typically, the blends will comprise two polymer types, however additional polymers can also be present.

“Biodegradable” as the term is used herein refers to polymers which can be ultimately degraded by a microbial process under environmental exposures to CO<sub>2</sub>, H<sub>2</sub>O and biomass. In certain cases, polymers such as polylactic acid are degraded by hydrolysis to individual monomer molecules which are then enzymatically decomposed to CO<sub>2</sub> and H<sub>2</sub>O by microorganisms. Examples of biodegradation processes include enzyme mediated hydrolytic and oxidative reactions that occur during composting.

“Compatibilizer” refers to a compound effective to provide a resin composition which exhibits improved compatibility compared to the same composition without the compatibilizer. Indicators of improved compatibility as described herein include, for example, increased impact strength and/or increased elongation at break.

PHAs are biodegradable polymers or copolymers having the following general structure for one or more of the repeating units:



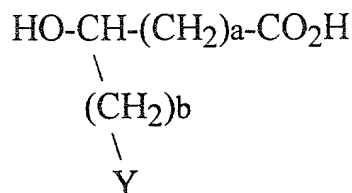
where a is 0 to 6, b is 0 to 15, Y is H, F, Cl, Br, CN, OH, CO<sub>2</sub>H, CO<sub>2</sub>R (where R is alkyl, benzyl etc.), methyl, cyclohexyl, phenyl, p-nitrophenoxy, p-cyanophenoxy, phenoxy, acetoxy, vinyl, 2-propyl, 2-butyl, 2-pentyl, 2-hexyl, etc., and n is an integer typically between about 10 and 25,000. The pendant groups of the repeating units may contain additional functionalization such as double bonds, epoxidized double bonds, hydroxyl groups, alkyl groups, alkenyl groups etc. or combinations thereof. The polymer main chain can contain up to 8 carbons in the repeating units and there may be additional functionalization in or on the main chain such as double bonds, alkyl groups, alkenyl groups, hydroxyl groups etc. or combinations thereof.

The PHAs can be produced synthetically, or in plant or microbial organisms. Most typically, it is a fermentation product, particularly of a microbiological process, whereby a microorganism lays down polyhydroxyalkanoate during normal or manipulated growth. Manipulation may be achieved by removing or failing to produce one or more nutrients necessary for cell multiplication. Numerous microbiological species are known in the art to be suitable for the production of polyhydroxyalkanoate polymers (see for example, Anderson and Dawes, Micro. Rev. 54 (4): 450-472, 1990). The microorganisms may be wild type or mutated or may have the necessary genetic material introduced into it, for example by any of the methods or recombinant DNA technology. It is to be emphasized that it is not necessary for the PHA-producing organism to be a microorganism, but at present such organisms are preferred.

The PHAs will typically have as constituents hydroxyalkanoates (HA) monomers which are substrates for PHA synthase enzymes. Biologically-produced PHA polymers are the product of PHA synthase microbial enzymes, and are produced in either a bacterial cell which naturally contains a PHA synthase, or in a bacterial or other cell type, for example a plant cell, which has been genetically engineered to express such an enzyme. The microbial PHA synthase enzymes have broad substrate ranges and are capable of incorporating a large number of HA monomers as constituents of biosynthetic PHA depending upon growth conditions, precursor substrate availability, and the source of the PHA synthase enzyme. The diversity in composition of biosynthetic PHA polymers is underscored by the fact that at least 91 HA monomers have been identified as substrates for PHA synthases (Steinbuchel, A. and Valentin, H. FEMS Micro. Letters 128 (1995) 219-228).

Suitable HA monomers can include those having the following formula:





where a is 0 to 6, b is 0 to 15 and Y is H, F, Cl, Br, CN, OH, CO<sub>2</sub>H, CO<sub>2</sub>R (where R is alkyl, benzyl etc.), methyl, cyclohexyl, phenyl, p-nitrophenoxy, p-cyanophenoxy, phenoxy, acetoxy, vinyl, 2-propyl, 2-butyl, 2-pentyl, 2-hexyl, etc. As in the above description, there may be additional functionalization in or on the pendant and/or main chains. The monomers or the lactones of the monomers can be homopolymerized or copolymerized either biochemically or synthetically to produce the polymer.

Preferred HA monomers include those where a= 1-4, b=0-15, and Y is H. More preferably, the monomers are those where a=1-2 and b=0-3, and Y is H.

In a most preferred polymer, the PHA is of formula (I) where a is 1, b is 1 or 2 and Y is H and especially where there are units with b = 1 and b = 2 copolymerized together. Suitable polyesters contain a preponderance of b = 1, especially with at least 70 mol % of such units, the balance being units in which b = 2. Polymer containing a = 1, b = 1, Y = H as the only units is polyhydroxybutyrate (PHB) polyester while that containing additionally b = 2 is polyhydroxybutyrate-co-valerate (PHBV).

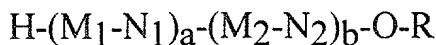
Other PHAs for use in the invention can be synthetically formed by approaches well known in the art, such as by lactone, lactide or glycolide ring-opening polymerization. Suitable lactones, lactides and glycolides include those that form biodegradable polylactones, polylactides and polyglycolides, respectively. Preferably, the polymer produced by ring-opening polymerization is polycaprolactone, formed from the ring opening polymerization of ε-caprolactone (6-hexanolactone).

The polymer blend compositions of the invention can comprise two or more structurally distinct PHAs as defined above, or can comprise non-PHA polymers in addition to PHAs. Non-PHA polymers suitable for the use in the blends of the present invention can include those which are to some extent biodegradable. In this way, when blended with a PHA, the resulting blend is capable of biodegradation. Furthermore, the selection of non-PHA polymer will depend upon the property or combination of properties sought to be optimized.

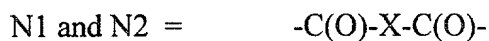
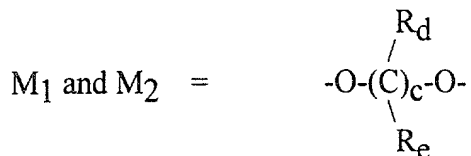
Generally, non-PHA polymers in the blends will include polyesters and copolyesters derived from various combinations of aliphatic dicarboxylic acids, aliphatic dicarboxylic acid chlorides, aliphatic dicarboxylic acid esters, and aliphatic diols or epoxides; polyurethanes made from such polyesters and copolyesters by reaction with a diisocyanate; aliphatic polycarbonates; polyanhydrides; polyester amides; polyester carbonates; polyester ethers; polyether carbonates; etc. Preferred non-PHA polymers for use in the invention include aliphatic polyesters and copolyesters, and polyester urethanes. More preferred non-PHA polymers include polycaprolactone (PCL, e.g. Tone 187P PCL, Union Carbide) and polybutylenesuccinate-adipate (PBSUA, e.g. Bionolle 3001 PBSUA, Showa High Polymer Co.).

For most applications and polymer combinations, the molecular weights of the polymers present in a blend will be in the range of 1000 to 2,000,000. The polymers can be blended in any manner and at any levels desired or suited for a particular application, and may vary depending upon the particular polymers selected. The relative ratio of polymers in a blend comprising two polymers can be, for example, from 99:1 to 1:99. For some applications, ratios of 90:10 to 10:90, or 80:20 to 20:80 may provide the most desired results.

The blends of the present invention contain one or more oligomeric/polymeric ester compounds (sometimes referred to herein as oligoesters), which can most typically be represented by the following formula:



where:



X is  $\text{C}_6\text{H}_4$  or  $(\text{CH}_2)_f$

a and b are independently 0 or an integer from 1 to 200;

c and f are independently integers from 1 to 30;

R is H or  $\text{C}_1$ - $\text{C}_{12}$  alkyl or branched alkyl; and

$\text{R}_d$  and  $\text{R}_e$  are H, or  $\text{C}_1$ - $\text{C}_{12}$  alkyl or branched alkyl and can vary independently with each  $(\text{C})_c$ .

The oligoesters are added to a blend in an amount effective to provide a resin composition which exhibits improved compatibility, as indicated by increased elongational and/or impact strengths, compared to the same composition without the oligoester. Typically, the oligomeric ester compounds of the invention will be present in a polymer blend at levels from 1 to 20, preferably from 2 to 15 wt.% of blend. The Mw of the oligomeric esters is generally in the range of 500 to 20,000, preferably 1000 to 10,000, most preferably 1500 to 7500.

Preferably, the compound is an oligomeric ester where f is 2 to 10. These include for example succinic (f= 2); glutaric (f=3); adipic (f=4); azelaic (f=7), and sebacic (f=8) ester compounds.

Most preferably, f is 4, i.e., the oligomeric ester is an oligomeric adipic ester, such as in poly(1,3-butylene glycol-co-1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\*S409A; Mw = 3700, available from Solutia Inc.), poly(neopentyl glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\*S433; Mw = 3500,

available from Solutia Inc.), poly(1,3-butylene glycol adipic acid) unterminated (Santicizer\*S430; Mw = 2500, available from Solutia Inc.), poly(1,3-butylene glycol adipic acid) unterminated (Santicizer\*S421; Mw = 1250, available from Solutia Inc.), poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol (Santicizer\*S438; Mw = 1900, available from Solutia Inc.), poly(neopentyl glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\*S435; Mw = 2500; available from Solutia Inc.), poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol (Santicizer \*431; Mw = 1200; available from Solutia Inc.), poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2 ethylhexanol (Santicizer \*S4212; Mw = 950; available from Solutia Inc.), poly (1,3-butylene glycol adipic acid) terminated with mixed fatty acids (Santicizer \*S405; Mw = 2000; available from Solutia Inc.), poly(1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\* S436; Mw = 3500; available from Solutia Inc.), poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer \*S449; Mw = 3700; available from Solutia Inc.), poly(1,4-butylene glycol adipic acid), or poly(1,4-butylene glycol-co-ethylene glycol adipic acid).

In a preferred embodiment of the invention, the blend composition comprises a PHA, polycaprolactone (PCL) and one or more oligomeric esters. The PCL in the blend is preferably present at a level of 10 to 40, more preferably 20 to 30 wt% in the blend, since age-related embrittlement is minimized at such levels. However, the skilled individual would recognize that other additives, particularly plasticizers, could vary the relative levels of PHA and PCL required in the blend to achieve the desired results.

In another preferred embodiment of the invention, the blend composition comprises a PHA, polybutylenesuccinate-adipate (PBSUA), and one or more oligomeric esters. The PBSUA in the blend is preferably present at a level of 10 to 40, more preferably 20 to 30 wt% in the blend, since age-related embrittlement is minimized at such levels. However, the skilled individual

would recognize that other additives, particularly plasticizers, could vary the relative levels of PHA and PBSUA required in the blend to achieve the desired results.

Preferred oligomeric esters according to these embodiments are oligomeric adipic esters such as poly(1,3-butylene glycol-co-1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\*S409A; Mw = 3700, available from Solutia Inc.), poly(neopentyl glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\*S433; Mw = 3500, available from Solutia Inc.), poly(1,3-butylene glycol adipic acid) unterminated (Santicizer\*S430; Mw = 2500, available from Solutia Inc.), poly(1,3-butylene glycol adipic acid) unterminated (Santicizer\*S421; Mw = 1250, available from Solutia Inc.), poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol (Santicizer\*S438; Mw = 1900, available from Solutia Inc.), poly(neopentyl glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\*S435; Mw = 2500; available from Solutia Inc.), poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol (Santicizer \*431; Mw = 1200; available from Solutia Inc.), poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2 ethylhexanol (Santicizer \*S4212; Mw = 950; available from Solutia Inc.), poly (1,3-butylene glycol adipic acid) terminated with mixed fatty acids (Santicizer \*S405; Mw = 2000; available from Solutia Inc.), poly(1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer\* S436; Mw = 3500; available from Solutia Inc.), poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol (Santicizer \*S449; Mw = 3700; available from Solutia Inc.), poly(1,4-butylene glycol adipic acid), or poly(1,4-butylene glycol-co-ethylene glycol adipic acid).

In addition to the blended polymers and the oligomeric esters described herein, other components can be present in the compositions of the invention, including the many polymer additives well known in the art. These can include, for example, nucleating agents, anti-blocking agents, lubricants, fillers, plasticizers, and other additives desired to optimize processing and/or product properties.

Prior to the present invention, it has been difficult to produce PHA shaped objects/articles that retain sufficient mechanical properties over their intended useful life. Instead, PHA-derived products rapidly embrittle within short periods of time, as indicated by their characteristic decline in elongational and impact properties. For example, elongation of molded PHBV bars containing 10 phr Santicizer S430 oligoester/polyester adipate (Solutia Inc.) dropped from 258% 3 hour after molding to 27% one day after molding to 10% sixty days after molding (see Example 5; Table 2). The situation was slightly improved by blending the PHBV with a structurally distinct PHA polymer, for example polycaprolactone (PCL). For PHBV bars containing 50 phr PCL, elongation was 235% one day after molding dropping to 26% after sixty days (see Example 1; Table 1). A similar trend was observed when the commonly used plasticizer acetyl-tributylcitrate (ATC) was added to the blend; elongation was 340% one day after molding, dropping to 50% after sixty days. Clearly, any improved elongational properties provided by these approaches were not sustainable and declined over time at unacceptable rates.

However, quite unexpectedly, when an oligomeric adipic ester according to the present invention is included in a blend of a PHA and another biodegradable polymer, excellent elongational properties are achieved and are maintained for at least 100 days after molding. For example, with PHBV containing 50 phr PCL and 10 phr of the oligoester Santicizer S430 (Solutia Inc.), elongation was 379% one day after molding, dropping only slightly to 348% after sixty days and remaining essentially unchanged after 100 days (see Examples 3 and 4; Table 1). These improvements in ductility and the reduced tendency to embrittlement for blends of PHAs containing oligoesters are clearly much greater than would be expected in view of the relatively modest improvements observed with a single PHA containing an oligoester or the results for blends of PHAs not containing an oligoester. Thus, the present invention provides compositions having exceptional elongational properties which can be sustained for lengths of time required in many commercial plastics applications.

Based on the results described herein, the compositions of this invention possess properties that would be desirable in numerous applications such as extrusion, molding, coating, spinning, blowing, thermoforming and calendaring processes or combinations of such processes. For example, increased melt strength of the blends compared with PHA alone is advantageous in the production of cast and blown films (both oriented and unoriented) for food packaging, grocery, lawn and trash bags, diaper backsheet and agricultural films having improved elongation to break sustainable over extended periods of time. The compositions are also suitable for use in extrusion and injection stretch blow molding operations, for example to prepare oriented bottles having improved impact strength over extended periods of time. Disposable food packaging articles such as tubs and containers, medical goods such as syringes, labware, and patient kits, as well as disposable plates, cups, knives and forks with improved tensile properties can also be made by injection molding operations using the compositions of the invention. The compositions can also be extruded into sheets and thermoformed into food packaging, plates, bowls etc. In addition, the blends can be melt spun into fibers for threads, ropes, nets as well as disposable nonwovens for medical applications. The skilled individual would recognize that the compositions of the invention are not limited by the above description, rather they are useful in essentially any application where increased melt strength, elongation, impact and/or aging characteristics are desired.

Preparation of the blend for use in melt extrusion of a shaped article can be performed using techniques known in the art. In one technique, the blend is prepared as a melt blend by melting of the first polymer, the second polymer, the oligoester, and optionally other additives, followed by pelletizing of the melt. The pellets of the blend are then used conventionally in melt extrusion techniques of forming shaped articles. Alternatively, the blend is prepared as a physical blend, by combining pellets, powders, or other formulations of the first polymer, the second polymer, the oligoester, and optionally other additives, in conventional melt extrusion techniques to produce shaped articles comprising the desired composition. The use of physical blends is

preferred, in that the number of melt steps required to prepare a shaped article comprising a composition of the present invention is reduced.

As used herein, the term "molecular weight", unless otherwise specified, refers to the weight average molecular weight (Mw) as opposed to the number average molecular weight (Mn). Most synthetic polymers have a broad distribution of molecular weights, and the molecular weights reported for such polymers represent averages, most frequently defined by Mw or Mn according to the following formulas:

$$M_w = \sum_i n_i M_i^2 / \sum_i n_i M_i$$

$$M_n = \sum_i n_i M_i / \sum_i n_i$$

where  $n_i$  = the number of molecules of molecular weight  $M_i$ . The most commonly used technique for determining Mw and Mn is by gel permeation chromatography (GPC) where values of Mw and Mn are obtained by calibration using monodisperse polystyrene fractions of known molecular weights. This method is capable of determining the entire molecular weight distribution of a polymer sample from which molecular weight averages can be determined. Other methods known in the art for determining Mw and Mn include osmometry, scattering and sedimentation (See for example, W. R. Sorensen & T. W. Campbell: Preparative Methods of Polymer Chemistry, Interscience Publishers, NY, 1961).

In accordance with yet another aspect of the present invention, there are provided polymer compositions comprising or consisting of a first biodegradable polymer comprising a poly-3-hydroxybutyrate-co-4-hydroxybutyrate (P3HB4HB) and a nucleant. It has been found that such compositions exhibit ductility, impact strength and aging characteristics improved to an unexpected and unpredictable extent.



P3HB4HB is a copolymer of 3-hydroxybutyrate (3HB) and 4-hydroxybutyrate (4HB), wherein the 3HB repeat unit has the structural formula above wherein  $Y=H$ ,  $b=1$ ,  $a=1$ , and  $n=1$ , and wherein the 4HB repeat unit has the structural formula above wherein  $Y=H$ ,  $b=0$ ,  $a=2$ , and  $n=1$ . The percentage of 4HB units in the P3HB4HB copolymer is preferably 1-99%, more preferably 5-50%, most preferably 8-20%. Especially preferred percentages are 8%, 9%, 10%, 11%, 12%, 13%, 14%, 15%, 16%, 17%, 18%, 19%, and 20%.

The nucleant can be any nucleant known to be effective in nucleating PHAs. A preferred nucleant is boron nitride. The concentration of nucleant can be any concentration known to be effective for the nucleation of PHAs using the nucleant. Typically, preferred concentrations of nucleant are 0.1 to 20 wt%, more preferably 1 to 10 wt%. For boron nitride, a most preferred concentration is 1 phr.

The composition of P3HB4HB and nucleant has favorable and unexpected elongation properties, and can be used in the applications described above for the blends.

The following examples are included to demonstrate preferred embodiments of the invention. It should be appreciated by those of skill in the art that the techniques disclosed in the examples which follow represent techniques discovered by the inventor to function well in the practice of the invention, and thus can be considered to constitute preferred modes for its practice. However, those of skill in the art should, in light of the present disclosure, appreciate that many changes can be made in the specific embodiments which are disclosed and still obtain a like or similar result without departing from the spirit and scope of the invention.

## EXAMPLES

### EXAMPLES 1-4: EFFECT OF PLASTICIZER ON TOUGHNESS OF PHBV/PCL BLENDS

**Example 1:** 100 phr PHBV (8%HV,  $M_w=895K$ ) powder was blended with 1 phr Boron nitride in a Papenmeier high speed mixer followed by addition of 50 phr Tone 787P (Union Carbide,

Mw=206K) corresponding to 33% PCL in the total blend. No plasticizer was added in this example. The powder /granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20), operated at 40 rpm using a temperature profile from 140 to 170°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 490K and a MFI(170°C/5 Kg)=3 g/10 min. Test bars were obtained by feeding the granules into 15 T Boy injection molding equipment using a temperature profile from 130 to 150°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 235% as molded, 176% after one day and 23% after 100 days. The results are presented in Table 1.

**Example 2:** 100 phr PHBV (8%HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papenmeier high speed mixer followed by addition of 10 phr Acetyl tributyl citrate (ATC) plasticizer under continuous agitation. After 5 minutes, 50 phr of PCL Tone 787P (Union Carbide, Mw=206K) granules were added under agitation, corresponding to 31% PCL in the total blend. The powder/granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20), operated at 40 rpm using a temperature profile from 140 to 170°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 530K and a MFI(170°C/5 Kg)=4.2 g/10 min. Test bars were obtained by feeding the granules into 15 T Boy injection molding equipment using a temperature profile from 130 to 150°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 340% as molded, 335% after one day and 60% after 100 days. The results are presented in Table 1.

**Example 3:** 100 phr PHBV (8%HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papenmeier high speed mixer followed by addition of 10 phr Santicizer 409A polymeric

plasticizer (1,3 butylene glycol-1,2 propylene glycol-adipic acid copolyester terminated with 2-ethylhexanol; Mw = 4200) under continuous agitation. After 5 minutes, 50 phr of PCL Tone 787P (Union Carbide, Mw=206K) granules were added under agitation, corresponding to 31% PCL in the total blend. The powder/granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20), operated at 40 rpm using a temperature profile from 140 to 170°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 495K and a MFI(170°C/5 Kg)=4.7 g/10 min. Test bars were obtained by feeding the granules into 15 T Boy injection molding equipment using a temperature profile from 130 to 150°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 333% as molded, 290% after one day and 245% after 100 days. Results are presented in Table 1.

**Example 4:** 100 phr PHBV (8%HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papenmeier high speed mixer followed by addition of 10 phr Santicizer 430 polymeric plasticizer (1,3 butylene glycol-adipic acid copolyester, unterminated; Mw=5500) under continuous agitation. After 5 minutes, 50 phr of PCL Tone 787P (Union Carbide, Mw=206K) granules were added under agitation, corresponding to 31% PCL in the total blend. The powder/granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20), operated at 40 rpm using a temperature profile from 140 to 170°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 600K and a MFI(170°C/5 Kg)=5.4 g/10 min. Test bars were obtained by feeding the granules into 15 T Boy injection molding equipment using a temperature profile from 130 to 150°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 417% as molded, 379% after one day and 348% after 60 days. Results are presented in Table 1.

**TABLE 1 - Summarized Results of Examples 1-4**

Example:	1	2	3	4
Plasticizer:	none	ATC	S409A	S430
% EB After:				
1 day	235	340	333	379
7 days	176	335	290	354
14 days	62	290	240	340
28 days	56	94	215	378
60 days	26	50	230	348
100 days	23	60	245	350

%EB = % elongation at break

ATC= Acetyl tributyl citrate

S409A= 1,3 butylene glycol-1,2 propylene glycol-adipic acid copolyester terminated with 2 ethylhexanol.

S430: 1,3 butyleneglycol-adipic acid copolyester

D400P Mw=895K: 100 phr Plasticizer: 10 phr

PCL Tone 787P: 50 phr Boron nitride nucleant: 1 phr

### EXAMPLES 5-9: EFFECT OF PCL LEVEL ON TOUGHNESS OF PHBV/S430/PCL BLENDS

**Example 5:** 100 phr PHBV (8%HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papanmeier high speed mixer followed by addition of 10 phr Santicizer 430 polyester polymeric plasticizer (1,3 butylene glycol adipic acid copolyester, unterminated; Mw=5500) under continuous agitation. The powder mixture was then fed into a Betol single screw extruder (25 mm; L/D=20), operated at 40 rpm using a temperature profile from 150 to 180°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 650K and a MFI(170°C/5 Kg)=4 g/10 min. Test bars were

obtained by feeding the granules into 15 T Boy injection molding equipment using a temperature profile from 140 to 160°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 258% as molded, 27% after one day and 10% after 60 days. Results are provided in Table 2.

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**Example 6:** 100 phr PHBV (8%HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papanmeier high speed mixer followed by addition of 10 phr Santicizer 430 polyester polymeric plasticizer under continuous agitation. After 5 minutes, 30 phr of PCL Tone 787P (Union Carbide) granules were added under agitation. The powder/granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20) operated at 40 rpm using a temperature profile from 150 to 180°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 600K and a MFI(170°C/5 Kg)=4.8 g/10 min. The granules were fed into 15 T Boy injection molding equipment using a temperature profile from 140 to 160°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 515% as molded, 454% after one day and 27% after 60 days. Results are presented in Table 2.

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**Example 7:** 100 phr PHBV (8%HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papanmeier high speed mixer followed by addition of 10 phr Santicizer 430 polyester polymeric plasticizer under continuous agitation. After 5 minutes, 40 phr of PCL Tone 787P (Union Carbide) granules were added under agitation. The powder/granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20), operated at 40 rpm using a temperature profile from 140 to 170°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 620K and a MFI(170°C/5 Kg)=4.3 g/10 min. The granules were fed into 15 T Boy injection molding equipment using a

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temperature profile from 130 to 150°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 411% as molded, 384% after one day and 335% after 60 days. Results are presented in Table 2.

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**Example 8:** 100 phr PHBV (8%HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papienmeier high speed mixer followed by addition of 10 phr Santicizer 430 polyester polymeric plasticizer under continuous agitation. After 5 minutes, 50 phr of PCL Tone 787P (Union Carbide) granules were added under agitation. The powder/granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20) operated at 40 rpm using a temperature profile from 140 to 170°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 600K and a MFI(170°C/5 Kg)=5.4 g/10 min. The granules were fed into 15 T Boy injection molding equipment using a temperature profile from 130 to 150°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 417% as molded, 379% after one day and 348% after 60 days. Results are presented in Table 2.

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**Example 9:** 100 phr PHBV (8%HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papienmeier high speed mixer followed by addition of 10 phr Santicizer 430 polyester polymeric plasticizer under continuous agitation. After 5 minutes, 70 phr of PCL Tone 787P (Union Carbide) granules were added under agitation. The powder/granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20), operated at 40 rpm using a temperature profile from 140 to 160°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 610K and a MFI(170°C/5 Kg)=4.8 g/10 min. The granules were fed into 15 T Boy injection molding equipment using a

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temperature profile from 130 to 140°C and a mold temperature around 40°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 284% as molded, 279% after one day and 270% after 60 days. Results are presented in Table 2.

**TABLE 2 - Summarized Results for Examples 5-9**

<b>Example:</b>	<b>5</b>	<b>6</b>	<b>7</b>	<b>8</b>	<b>9</b>
<b>PCL (phr)</b>	<b>0</b>	<b>30</b>	<b>40</b>	<b>50</b>	<b>70</b>
<b>PCL% in blend</b>	<b>0</b>	<b>21</b>	<b>26</b>	<b>31</b>	<b>39</b>
<b>% EB After:</b>					
<b>3 hrs</b>	<b>258</b>	<b>515</b>	<b>411</b>	<b>417</b>	<b>284</b>
<b>1 day</b>	<b>27</b>	<b>454</b>	<b>384</b>	<b>379</b>	<b>279</b>
<b>7 days</b>	<b>12</b>	<b>242</b>	<b>363</b>	<b>354</b>	<b>258</b>
<b>14 days</b>	<b>12</b>	<b>221</b>	<b>341</b>	<b>347</b>	<b>272</b>
<b>28 days</b>	<b>10</b>	<b>133</b>	<b>365</b>	<b>378</b>	<b>243</b>
<b>60 days</b>	<b>10</b>	<b>27</b>	<b>335</b>	<b>348</b>	<b>270</b>
<b>Notched Izod Impact(KJ/m2)</b>	<b>3.4</b>	<b>3.6</b>	<b>5.7</b>	<b>5.4</b>	<b>26.4</b>

%EB = % elongation at break  
D400P Mw=895K: 100 phr S430 polyester plasticizer: 10 phr  
PCL Tone 787P: variable Boron nitride nucleant: 1 phr

# **EXAMPLES 10-13: EFFECT OF PCL LEVEL ON ELONGATION OF PHBV/S430/PCL BLOWN FILMS**

**Example 10:** The granules obtained as described in example 5 based on 100 phr PHBV, 1 phr BN and 10 phr S430 were fed into a 22mm single screw Formac film blowing extruder fitted with a 50 mm circular die (die gap=1mm) using a temperature profile from 155 to 165 °C and a screw speed

around 12 rpm. The extruded tubular film which cooled and blown with air to a 70 mm diameter bubble produced after collapsing between nip rolls a film with an average thickness of 70 microns characterized by a tensile strength after one day around 26 MPa and an elongation at break of 13%. After 21 days, the tensile strength was 27 MPa and the elongation was 6%. Results are presented in Table 3.

**Example 11:** The granules obtained as described in example 6 based on 100 phr PHBV, 1 phr BN, 10 phr S430, 0.15 phr anti-blocking agent and 30 phr PCL were fed into a 22mm single screw Formac film blowing extruder fitted with a 50 mm circular die (die gap=1mm) using a temperature profile from 155 to 165 °C and a screw speed around 13 rpm. The extruded tubular film which cooled and blown with air to a 65 mm diameter bubble produced after collapsing between nip rolls a film with an average thickness of 85 microns characterized by a tensile strength after one day around 32 MPa and an elongation at break of 800%. After 21 days, the tensile strength was 32 MPa and the elongation was 750%. Results are presented in Table 3.

**Example 12:** The granules obtained as described in example 7 based on 100 phr PHBV, 1 phr BN, 10 phr S430, 0.15 phr anti-blocking agent and 40 phr PCL were fed into a 22mm single screw Formac film blowing extruder fitted with a 50 mm circular die (die gap=1mm) using a temperature profile from 155 to 165 °C and a screw speed around 13 rpm. The extruded tubular film which cooled and blown with air to a 65 mm diameter bubble produced after collapsing between nip rolls a film with an average thickness of 90 microns characterized by tensile strength after one day around 36 MPa and an elongation at break of 970%. After 21 days, the tensile strength was 36 MPa and the elongation was 900%. Results are presented in Table 3.

**Example 13:** The granules obtained as described in example 8 based on 100 phr PHBV, 1 phr BN, 10 phr S430, 0.15 phr anti-blocking agent and 50 phr PCL were fed into a 22mm single screw Formac film blowing extruder fitted with a 50 mm circular die (die gap=1mm) using a temperature profile from 155 to 165 °C and a screw speed around 13 rpm. The extruded tubular film which



cooled and blown with air to a 65 mm diameter bubble produced after collapsing between nip rolls a film with an average thickness of 85 microns characterized by tensile strength after one day around 35 MPa and an elongation at break of 925%. After 21 days, the tensile strength was 36 MPa and the elongation was 790%. Results are presented in Table 3.

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**TABLE 3 - Summarized Results for Examples 10-13**

10	<b>Example:</b>	<b>10</b>	<b>11</b>	<b>12</b>	<b>13</b>
	<b>PCL (phr)</b>	<b>0</b>	<b>30</b>	<b>40</b>	<b>50</b>
	<b>PCL% in blend</b>	<b>0</b>	<b>21</b>	<b>26</b>	<b>31</b>
15	<b>Film thickness (μm)</b>	<b>70</b>	<b>85</b>	<b>90</b>	<b>85</b>
	<b>TSB (MPa)</b>				
	<b>After 1 day</b>	<b>26</b>	<b>32</b>	<b>36</b>	<b>35</b>
20	<b>7 days</b>	<b>27</b>	<b>33</b>	<b>35</b>	<b>32</b>
	<b>21 days</b>	<b>27</b>	<b>32</b>	<b>36</b>	<b>36</b>
	<b>% EB After:</b>				
25	<b>1 day</b>	<b>13</b>	<b>800</b>	<b>970</b>	<b>925</b>
	<b>7 days</b>	<b>5</b>	<b>790</b>	<b>950</b>	<b>870</b>
	<b>21days</b>	<b>6</b>	<b>750</b>	<b>900</b>	<b>790</b>

TSB = tensile strength at break %EB = % elongation at break  
D400P Mw=895K: 100 phr Stearamide anti-blocking: 0.15 phr  
Boron nitride nucleant: 1 phrPCL Tone 787P: variable  
S430 polyester plasticizer: 10 phr

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35 **EXAMPLES 14-17: EFFECT OF PCL LEVEL ON ELONGATION OF  
PHBV/S430/PCL CAST FILMS**

All cast films were obtained on a Dr Collin cast film line consisting in a 45mm diameter, 25 L/D single screw extruder fitted with a 500mm wide flat die with 1mm die gap. The temperature profile of the barrel was set from 145°C to 155°C. The adaptor temperature was set at 156°C while the die temperatures were set at 170°C. The extruded film was deposited on a temperature regulated metal chill roll (T1=75°C)) followed by nip rolls composed of one rubber roll exercising a pressure on a second heated metal chill roll (T2=45°C). The three rolls had a diameter of 150mm. The line was followed by a series of small "free" rolls up to a pulling/winder roll arrangement. Different film thickness were obtained by varying the screw speed (output) of the extruder and the chill roll speed.

**Example 14:** Granules obtained as described in example 6 based on 100 phr PHBV, 1 phr BN, 10 phr S430, 0.15 phr anti-blocking agent and 30 phr PCL were fed into the Dr Collin cast film line described here above. Using a screw speed of 20 rpm and a pulling speed of 2.5 m/min, a 70 µm thick, 300 mm wide cast film was obtained. Tensile testing was carried out on stamped dog-bone bars (4 mm wide, 20 mm gauge length and 10 mm/min crosshead speed). The film was characterized by a tensile strength at break (in machine direction) after one week around 26 MPa and an elongation at break of 480%. After 100 days, the elongation was 32%. Results are presented in Table 4.

**Example 15:** Granules obtained as described in example 6 based on 100 phr PHBV, 1 phr BN, 10 phr S430, 0.15 phr anti-blocking agent and 30 phr PCL were fed into the Dr Collin cast film line described here above. Using a screw speed of 25 rpm and a pulling speed of 2.0 m/min, a 120 µm thick, 360 mm wide cast film was obtained. Tensile testing was carried out on stamped dog-bone bars (4 mm wide, 20 mm gauge length and 10 mm/min crosshead speed). The film was characterized by a tensile strength at break (in machine direction) after one week around 25 MPa and an elongation at break of 570%. After 100 days, the elongation was 40%. Results are presented in Table 4.

**Example 16:** Granules obtained as described in example 7 based on 100 phr PHBV, 1 phr BN, 10 phr S430, 0.15 phr anti-blocking agent and 40 phr PCL were fed into the Dr Collin cast film line described here above. Using a screw speed of 20 rpm and a pulling speed of 2.1 m/min, a 110  $\mu$ m thick, 300 mm wide cast film was obtained. Tensile testing was carried out on stamped dog-bone bars (4 mm wide, 20 mm gauge length and 10 mm/min crosshead speed). The film was characterized by a tensile strength at break (in machine direction) after one week around 35 MPa and an elongation at break of 780%. After 100 days, the elongation was 700%. Results are presented in Table 4.

**Example 17:** Granules obtained as described in example 7 based on 100 phr PHBV, 1 phr BN, 10 phr S430, 0.15 phr anti-blocking agent and 40 phr PCL were fed into the Dr Collin cast film line described here above. Using a screw speed of 30 rpm and a pulling speed of 2.0 m/min, a 145  $\mu$ m thick, 360 mm wide cast film was obtained. Tensile testing was carried out on stamped dog-bone bars (4 mm wide, 20 mm gauge length and 10 mm/min crosshead speed). The film was characterized by a tensile strength at break (in machine direction) after one week around 31 MPa and an elongation at break of 800%. After 100 days, the elongation was 620%. Results are presented in Table 4.

**TABLE 4 - Summarized Results for Examples 14-17**

Example	14	15	16	17
PCL (phr)	30		40	
PCL(%)		21		26
Film thickness( $\mu$ )	70	120	110	145
EB%				
After 7 days	480	570	780	800
After 30 days	160	72	760	770
After 60 days	65	63	740	730
After 100 days	32	40	700	620

EB= Elongation at break

Composition: D400P Mw=895K: 100 phr

Boron nitride nucleant: 1 phr

S430 polyester plasticizer: 10 phr

Stearamide anti-blocking: 0.15 phr

PCL Tone P-787: variable

## EXAMPLES 18-19: EFFECT OF PLASTICIZER ON TOUGHNESS OF PHBV/PBSUA BLENDS

**Example 18:** 100 phr PHBV (8% HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papenmeier high speed mixer, followed by addition of 10 phr S430 PBGA plasticizer and 40 phr Bionolle 3001 PBSUA granules (Union Carbide, Mw=204K), corresponding to 26% PBSUA in the total blend.

The powder/granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20) operated at 40 rpm using a temperature profile from 140 to 170°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The output was 3.4 Kg/hr. The granules obtained had a Mw around 650°K and a MFI (170°C/5 Kg)=3.5 g/10 min.

Test bars were obtained by feeding the granules into a 15 T Boy injection molding equipment using a temperature profile from 130 to 150°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 320% as molded, 310% after 30 days, and 65% after 90 days. Results are presented in Table 5.

**Example 19:** 100 phr PHBV (8% HV, Mw=895K) powder was blended with 1 phr Boron nitride in a Papenmeier high speed mixer, followed by addition of 10 phr S430 PBGA plasticizer

and 50 phr Bionolle 3001 PBSUA granules (Union Carbide, Mw=204K), corresponding to 31% PBSUA in the total blend.

The powder/granule mixture was then fed into a Betol single screw extruder (25 mm; L/D=20) operated at 40 rpm using a temperature profile from 140 to 170°C and a screw speed of 40 rpm, and fitted with a 4 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The output was 3.3 Kg/hr. The granules obtained had a Mw around 620°K and a MFI (170°C/5 Kg)=3.6 g/10 min.

Test bars were obtained by feeding the granules into a 15 T Boy injection molding equipment using a temperature profile from 130 to 150°C and a mold temperature around 55°C. Tensile testing on molded bars (5X2mm section, 42 mm gauge length, 10 mm:min crosshead speed) gave elongation at break of 360% as molded, 390% after 30 days, and 340% after 90 days. Results are presented in Table 5.

**TABLE 5 - Summarized Results for Examples 18-19**

Example	18	19
PBSUA (phr)	40	50
PBSUA% in blend	26	31
% Elongation at break		
After 3 hrs	320	360
3 days	330	450
7 days	310	420
15 days	315	440
30 days	310	400
60 days	100	335
90 days	65	345

Composition: D400P Mw=895K: 100 phr  
Boron nitride nucleant: 1 phr  
S430 polyester plasticizer: 10 phr  
Bionolle 3001 PBSUA: variable

**EXAMPLES 20-23: EFFECT OF PBSUA LEVEL ON ELONGATION OF  
PHBV/S430/PBSUA BLOWN FILMS:**

5 All blown films were obtained on a 20 mm diameter Brabender/Haake single screw extruder fitted with a circular die and a 1 meter high blowing tower equipped with two 80 mm diameter nip rolls. The film width and thickness was adjusted by varying the screw speed of the extruder, the pulling rate of the tubular film and the diameter of the bubble.

10 **Example 20:** Granules obtained as described in example 18 based on 100 phr PHBV, 1 phr BN, 10 phr S430, and 40 phr Bionolle 3001 PBSUA were extruded through a 20 mm single screw extruder fitted with a 25 mm circular die using a temperature profile from 160 to 170°C. At a screw speed of 15 rpm and a pulling rate of 1.5 m/min., the extruded tubular preform, which was cooled and blown with air to a 25 mm diameter bubble, produced after collapsing between two nip  
15 rolls a film with a width of 80 mm and a thickness of 65 µm. Tensile testing stamped dog-bone bars (4 mm wide, 20 mm gauge length and 10 mm/min crosshead speed) gave an elongation at break of 670% after 5 days and 720% after 90 days. Results are presented in Table 6.

20 **Example 21:** Granules obtained as described in example 18 based on 100 phr PHBV, 1 phr BN, 10 phr S430, and 40 phr Bionolle 3001 PBSUA were extruded through a 20 mm single screw extruder fitted with a 25 mm circular die using a temperature profile from 160 to 170°C. At a screw speed of 15 rpm and a pulling rate of 1.5 m/min, the extruded tubular preform, which was cooled and blown with air to a 20 mm diameter bubble, produced after collapsing between two nip  
25 rolls a film with a width of 65 mm and a thickness of 130 µm. Tensile testing stamped dog-bone bars (4 mm wide, 20 mm gauge length and 10 mm/min crosshead speed) gave an elongation at break of 590% after 5 days and 620% after 90 days. Results are presented in Table 6.

**Example 22:** Granules obtained as described in example 19 based on 100 phr PHBV, 1 phr BN, 10 phr S430, and 50 phr Bionolle 3001 PBSUA were extruded through a 20 mm single screw

extruder fitted with a 25 mm circular die using a temperature profile from 165 to 170°C. At a screw speed of 20 rpm and a pulling rate of 2 m/min, the extruded tubular preform, which was cooled and blown with air to a 25 mm diameter bubble, produced after collapsing between two nip rolls a film with a width of 85 mm and a thickness of 80 µm. Tensile testing stamped dog-bone bars (4 mm wide, 20 mm gauge length and 10 mm/min crosshead speed) gave an elongation at break of 610% after 5 days and 805% after 90 days. Results are presented in Table 6.

**Example 23:** Granules obtained as described in example 19 based on 100 phr PHBV, 1 phr BN, 10 phr S430, and 50 phr Bionolle 3001 PBSUA were extruded through a 20 mm single screw extruder fitted with a 25 mm circular die using a temperature profile from 165 to 170°C. At a screw speed of 15 rpm and a pulling rate of 1 m/min, the extruded tubular preform, which was cooled and blown with air to a 18 mm diameter bubble, produced after collapsing between two nip rolls a film with a width of 55 mm and a thickness of 180 µm. Tensile testing stamped dog-bone bars (4 mm wide, 20 mm gauge length and 10 mm/min crosshead speed) gave an elongation at break of 1080% after 5 days and 700% after 90 days. Results are presented in Table 6.

**TABLE 6 - Summarized Results for Examples 20-23**

Example	20	21	22	23
PBSUA (phr)		40		50
PBSUA (%)		26		31
Film thickness(µm)	65	130	80	180
EB%				
After 5 days	670	590	610	1080
After 30 days	700	580	800	840
After 60 days	725	610	780	750
After 90 days	720	620	805	700

EB= Elongation at break

Composition: D-400P Mw=895K: 100 phr  
Boron nitride nucleant: 1 phr  
S430 polyester plasticizer: 10 phr  
Bionolle 3001 PBSUA: variable

## EXAMPLE 24: TOUGHNESS OF P3HB-4HB BLEND

**Example 24:** 100 phr P3HB-4HB (13% 4HB, Mw=1180K) powder was blended with 1 phr Boron nitride in a Papenmeier high speed mixer. The powder mixture was then fed into a Haake single screw extruder (20 mm; L/D=25; Compression ratio 3:1) using a temperature profile from 155 to 185°C and a screw speed of 40 rpm, and fitted with a 3 mm single strand die. The extrudate was cooled in a water bath maintained at 60°C+/-5°C using a thermoregulator and then cut into granules in a pelletizer. The granules obtained had a Mw around 800K.

Tensile test bars were obtained by hot pressing the granules between two Teflon coated metal plates heated at 180°C and stamping dog-bone bars 4 mm wide with a 20 mm gauge length. Tensile testing gave elongation at break of 1080% about 3 hr after molding and 920% after 100 days. Results are presented in Table 7.

**TABLE 7 - Summarized Results for Example 24**

Example	24
<b>Elongation at break on hot pressed films</b>	
After 3 hrs	1080%
After 1 day	1100%
After 30 days	850%
After 75 days	920%
Composition: P3HB-4HB(13%4HB; Mw=1180K): 100 phr Boron nitride nucleant: 1 phr	

## EXAMPLES 25-26: EFFECT OF FILM THICKNESS ON ELONGATION OF P3HB-4HB BLOWN FILMS:

All blown films were obtained on a 20 mm diameter Brabender/Haake single screw extruder fitted with a circular die and a 1 meter high blowing tower equipped with two 80 mm



diameter nip rolls. The film width and thickness was adjusted by varying the screw speed of the extruder, the pulling rate of the tubular film and the diameter of the bubble.

**Example 25:** Granules obtained as described in example 24 based on 100 phr P3HB-4HB and 1 phr BN were extruded through a 20 mm single screw extruder fitted with a 25 mm circular die using a temperature profile from 170 to 180°C. At a screw speed of 15 rpm and a pulling rate of 1 m/min, the extruded tubular preform, which was cooled and blown with air to a 22 mm diameter bubble, produced after collapsing between two nip rolls a film with a width of 70 mm and a thickness of 85  $\mu\text{m}$ . Tensile testing on dog-bone samples stamped from the film in the machine direction (4mm wide, 20 mm gauge length) gave an elongation at break of 710% after 5 days and 560% after 90 days. Results are presented in Table 9.

**Example 26:** Granules obtained as described in example 24 based on 100 phr P3HB-4HB and 1 phr BN were extruded through a 20mm single screw extruder fitted with a 25 mm circular die using a temperature profile from 170 to 180°C. At a screw speed of 15 rpm and a pulling rate of 1 m/min, the extruded tubular preform, which was cooled and blown with air to a 18 mm diameter bubble, produced after collapsing between two nip rolls a film with a width of 55 mm and a thickness of 130  $\mu\text{m}$ . Tensile testing on dog-bone samples stamped from the film in the machine direction (4mm wide, 20 mm gauge length) gave an elongation at break of 710% after 5 days and 560% after 90 days. Results are presented in Table 9.

**TABLE 9 - Summarized Results for Examples 25-26**

5	<b>Example</b>	<b>25</b>	<b>26</b>
	<b>Film thickness (<math>\mu\text{m}</math>)</b>	<b>85</b>	<b>130</b>
	<b>EB%</b>		
	<b>After 5 days</b>	<b>710</b>	<b>780</b>
	<b>After 30 days</b>	<b>640</b>	<b>620</b>
10	<b>After 60 days</b>	<b>620</b>	<b>630</b>
	<b>After 90 days</b>	<b>560</b>	<b>620</b>

EB= Elongation at break

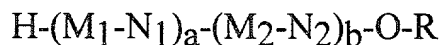
Composition: P3HB-4HB: 100 phr

Boron nitride nucleant: 1 phr

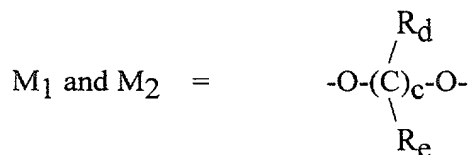
15 All of the compositions and methods disclosed and claimed herein can be made and executed without undue experimentation in light of the present disclosure. While the invention has been described in terms of preferred embodiments, it will be apparent to those of skill in the art that variations may be applied to the steps or in the sequence of steps of the methods described herein without departing from the concept, spirit and scope of the invention. More specifically, it will be apparent that certain agents which are both chemically and physiologically related may be substituted for the agents described herein while the same or similar results would be achieved. All such similar substitutes and modifications apparent to those skilled in the art are deemed to be within the spirit, scope and concept of the invention as defined by the appended claims.

**WHAT IS CLAIMED IS:**

1. A polymer composition comprising a first biodegradable polymer comprising a polyhydroxyalkanoate (PHA), a second biodegradable polymer different from the first polymer, and one or more oligomeric esters.
2. The composition of claim 1 wherein the oligomeric ester has the structural formula:



where:



X is  $\text{C}_6\text{H}_4$  or  $(\text{CH}_2)_f$

a and b are independently 0 or an integer from 1 to 200;

c and f are independently integers from 1 to 30;

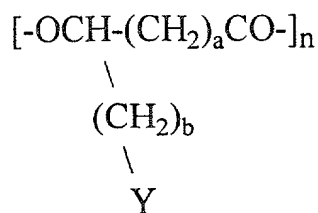
R is H or  $\text{C}_1$ - $\text{C}_{12}$  alkyl or branched alkyl; and

$\text{R}_d$  and  $\text{R}_e$  are H, or  $\text{C}_1$ - $\text{C}_{12}$  alkyl or branched alkyl and can vary independently with each  $(\text{C})_c$ .

3. The composition of claim 2 wherein f is 2 to 10.
4. The composition of claim 2 wherein f is 4.
5. The composition of claim 1 wherein the oligomeric ester is poly(1,3-butylene glycol-co-1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol, poly(neopentyl glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,3-butylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,3-butylene glycol adipic acid)

unterminated, poly(1,3-butylene glycol adipic acid) unterminated, poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol, poly(neopentyl glycol adipic acid) terminated with 2-ethylhexanol, poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol, poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2 ethylhexanol, poly(1,3-butylene glycol adipic acid) terminated with mixed fatty acids, poly(1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,4-butylene glycol adipic acid), or poly(1,4-butylene glycol-co-ethylene glycol adipic acid).

6. The composition of claim 1 wherein the oligomeric ester has a molecular weight in the range of 500 to 20,000.
7. The composition of claim 1 wherein the oligomeric ester has a molecular weight in the range of 1500 to 7500.
8. The composition of claim 1 wherein the oligomeric ester is present at levels from 1 to 20 wt.% of the blend.
9. The composition of claim 1 wherein the oligomeric ester is present at levels from 2 to 15 wt.% of the blend.
10. The composition of claim 1 wherein the blend comprises two polymers having a relative weight ratio in the blend of 99:1 to 1:99.
11. The composition of claim 1 wherein the blend comprises two polymers having a relative weight ratio in the blend of 80:20 to 20:80.
12. The composition of claim 1 wherein the PHA has the structural formula:



where a= 1-4, b=0-15, Y is H, and n is an integer.

13. The composition of claim 1 wherein the PHA is polyhydroxybutyrate or polyhydroxybutyrate-co-valerate.

14. The composition of claim 1 wherein said second polymer is a polyester or copolyester derived from aliphatic dicarboxylic acids or anhydrides, aliphatic dicarboxylic acid chlorides, aliphatic dicarboxylic acid esters, and aliphatic diols or epoxides; a polyurethane made from said polyesters and copolyesters by reaction with a diisocyanate; an aliphatic polycarbonate; a polyanhydride; a polyester amide; a polyester carbonate; a polyester ether; a polyether carbonate, or combinations thereof.

15. The composition of claim 1 wherein one of the polymers or copolymers in the blend is formed from lactone, lactide or glycolide ring-opening polymerization.

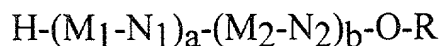
16. A polymer composition comprising a polyhydroxyalkanoate (PHA), a polycaprolactone (PCL), and one or more oligomeric esters.

17. The composition of claim 16 wherein the PHA is polyhydroxybutyrate (PHB) or polyhydroxybutyrate-co-valerate (PHBV).

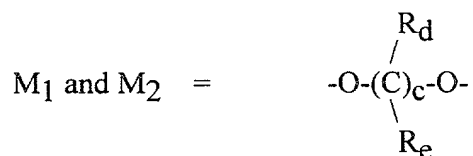
18. The composition of claim 16 wherein the PCL is present at 10 to 40 wt% in the blend.

19. The composition of claim 16 wherein the PCL is present at 20 to 30 wt% in the blend.

20. The composition of claim 16 wherein the oligomeric ester has the structural formula:



where:



X is  $\text{C}_6\text{H}_4$  or  $(\text{CH}_2)_f$

a and b are independently 0 or an integer from 1 to 200;

c and f are independently integers from 1 to 30;

R is H or  $\text{C}_1$ - $\text{C}_{12}$  alkyl or branched alkyl; and

$\text{R}_d$  and  $\text{R}_e$  are H, or  $\text{C}_1$ - $\text{C}_{12}$  alkyl or branched alkyl and can vary independently with each  $(\text{C})_c$ .

21. The composition of claim 20 wherein f is 2 to 10.

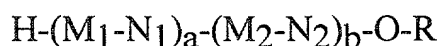
22. The composition of claim 20 wherein f is 4.

23. The composition of claim 16 wherein the oligomeric ester is poly(1,3-butylene glycol-co-1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol, poly(neopentyl glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,3-butylene glycol adipic acid) unterminated, poly(1,3-butylene glycol adipic acid) unterminated, poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol, poly(neopentyl glycol adipic acid) terminated with 2-ethylhexanol, poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol, poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2 ethylhexanol, poly(1,3-butylene glycol adipic acid) terminated with mixed fatty acids, poly(1,2-

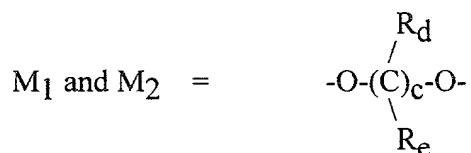
propylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,4-butylene glycol adipic acid), or poly(1,4-butylene glycol-co-ethylene glycol adipic acid).

24. A method of producing a shaped polymeric object comprising melting a composition comprising a polyhydroxyalkanoate (PHA), a second biodegradable polymer different from the first polymer, and one or more oligomeric esters, and producing a shaped object therefrom by extrusion, molding, coating, spinning, blowing, thermoforming or calendaring processes or combinations of the processes.

25. The method of claim 24 wherein the oligomeric ester has the structural formula:



where:



X is  $-C_6H_4-$  or  $-(CH_2)_f$

a and b are independently 0 or an integer from 1 to 200;

c and f are independently integers from 1 to 30;

R is H or  $C_1-C_{12}$  alkyl or branched alkyl; and

$R_d$  and  $R_e$  are H, or  $C_1-C_{12}$  alkyl or branched alkyl and can vary independently with each  $(C)_c$ .

26. The method of claim 24 wherein f is 2 to 10.

27. The method of claim 24 wherein f is 4.

28. The method of claim 24 wherein the oligomeric ester is poly(1,3-butylene glycol-co-1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol, poly(neopentyl glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,3-butylene glycol adipic acid) unterminated, poly(1,3-butylene glycol adipic acid) unterminated, poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol, poly(neopentyl glycol adipic acid) terminated with 2-ethylhexanol, poly(1,2-propylene glycol adipic acid-co-phthalic acid) terminated with 2-ethylhexanol, poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,3-butylene glycol adipic acid) terminated with mixed fatty acids, poly(1,2-propylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,2-propylene glycol-co-1,4-butylene glycol adipic acid) terminated with 2-ethylhexanol, poly(1,4-butylene glycol adipic acid), or poly(1,4-butylene glycol-co-ethylene glycol adipic acid).

29. The method of claim 24 wherein the Mw of the oligomeric ester is 500 to 20000.

30. The method of claim 24 wherein the PHA is polyhydroxybutyrate (PHB) or polyhydroxybutyrate-co-valerate (PHBV).

31. The method of claim 24 wherein the second polymer is polycaprolactone.

32. The method of claim 31 wherein the polycaprolactone is present at 10 to 40 wt.% of the blend.

33. A shaped object made according to claim 24.

34. A shaped object made according to claim 25.



35. A shaped object made according to claim 26.
36. A shaped object made according to claim 27.
37. A shaped object made according to claim 28.
38. A shaped object made according to claim 29.
39. A shaped object made according to claim 30.
40. A shaped object made according to claim 31.
41. A shaped object made according to claim 32.
42. A polymer composition comprising poly-3-hydroxybutyrate-co-4-hydroxybutyrate (P3HB4HB) and a nucleant.
43. The composition of claim 42 wherein the nucleant is boron nitride.
44. The composition of claim 42 wherein the nucleant is present at levels from 0.1 to 20 wt% of the blend.
45. The composition of claim 42 wherein the nucleant is present at levels from 1 to 10 wt% of the blend.
46. A method of producing a shaped polymeric object comprising melting a composition comprising poly-3-hydroxybutyrate-co-4-hydroxybutyrate (P3HB4HB) and a nucleant, and producing a shaped object therefrom by extrusion, molding, coating, spinning, blowing, thermoforming or calendaring processes or combinations of the processes.

47. The method of claim 46 wherein the nucleant is boron nitride.
48. A shaped object made according to claim 46.
49. A shaped object made according to claim 47.

### ABSTRACT

Biodegradable polymer blend compositions are provided which contain oligomeric esters. The oligoester compounds can compatibilize blends of two or more biodegradable polymers resulting in excellent ductility and reduced tendency to embrittlement of products produced from therefrom. In a preferred embodiment of the invention, the blend composition comprises a PHA, polycaprolactone (PCL) and one or more oligomeric esters. In another preferred embodiment of the invention, the blend composition comprises a PHA, polybutylenesuccinate-adipate (PBSUA), and one or more oligomeric esters.

**PATENT**

**IN THE UNITED STATES PATENT AND TRADEMARK OFFICE**

**In re Application of:**

**JAWED ASRAR  
JEAN R. PIERRE**

**Serial No.: 09/179,780**

**Filing Date: October 27, 1998**

**For: POLYMER BLENDS CONTAINING  
POLYHYDROXYALKANOATES AND  
COMPOSITIONS WITH GOOD  
RETENTION OF ELONGATION**

**Atty. Dkt: MOBT:189—  
38-21(15035)B**

**CORRESPONDENCE ADDRESS  
ELECTION UNDER 37 C.F.R. §§ 3.71 and 3.73  
AND POWER OF ATTORNEY**

**Assistant Commissioner for Patents  
Washington, D.C. 20231**

**Sir:**

**Please direct all communications as follows:**

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The undersigned, being Assignee of the entire interest in the above-identified application by virtue of an Assignment recorded in the United States Patent and Trademark Office as set forth below, hereby elects, under 37 C.F.R. § 3.71, to prosecute the application to the exclusion of the inventor(s).

The Assignee hereby revokes any previous Powers of Attorney and appoints:

T. K. Ball, Reg. No. 42,287; S. Christopher Bauer, Reg. No. 42,305; George R. Beck, Reg. No. 21,180; Dennis A. Bennett, Reg. No. 34,547; Jon H. Beusen, Reg. No. 30,610; Gary M. Bond, Reg. No. 29,283; Grace L. Bonner, Reg. No. 32,963; Joseph W. Bulock, Reg. No. 37,103; Alan E. Dow, Reg. No. 35,123; James C. Forbes, Reg. No. 39,457; Dennis R. Hoerner, Jr., Reg. No. 30,914; Jeffrey M. Hoster, Reg. No. 32,240; J. Timothy Keane, Reg. No. 27,808; Thomas E. Kelley, Reg. No. 29,938; Robert M. Kennedy, Reg. No. 28,026; Cynthia S. Kovacevic, Reg. No. 35,578; Lawrence M. Lavin, Jr., Reg. No. 30,768; Thomas P. McBride, Reg. No. 32,706; Scott J. Meyer, Reg. No. 25,275; Stasia L.

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Ogden, Reg. No. 36,228; Michael J. Roth, Reg. No. 29,342; Donna E. Scherer, Reg. No. 34,719; Carl J. Schwedler, Reg. No. 36,924; Alan L. Scrivner, Reg. No. 43,104; Richard H. Shear, Reg. No. 26,583; Brian K. Stierwalt, Reg. No. 33,213; and Roger A. Williams, Reg. No. 27,679; each an attorney or patent agent with MONSANTO COMPANY, so long as they remain with such company,

and

John F. Lynch, Reg. No. 22,504; J. Paul Williamson, Reg. No. 29,600; John D. Norris, Reg. No. 28,246; Patricia A. Kammerer, Reg. No. 29,775; Stephen H. Cagle, Reg. No. 26,445; Melinda L. Patterson, Reg. No. 33,062; Susan K. Knoll, Reg. No. 33,254; Steven Z. Szczepanski, Reg. No. 27,957; Barbara S. Kitchell, Reg. No. 33,928; Mary Jo Boldingh, Reg. No. 34,713; L. Gene Spears, Reg. No. 35,369; Janelle D. Waack, Reg. No. 36,300; Michael E. Lee, Reg. No. 38,949; Harold N. Wells, Reg. No. 26,044; Carter J. White, Reg. No. 41,374, and Raymund Eich, Reg. No. 42,508; each an attorney or patent agent with the law firm of ARNOLD, WHITE & DURKEE, as its attorney so long as they remain with such law firm,

with full power of substitution and revocation, to prosecute the application, to make alterations and amendments therein, to transact all business in the Patent and Trademark Office in connection therewith, to receive any Letters Patent, and for one year after issuance of such Letters Patent to file any request for a certificate of correction that may be deemed appropriate.

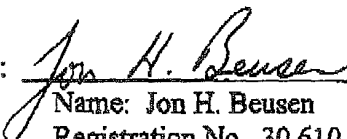
Pursuant to 37 C.F.R. § 3.73, the undersigned has reviewed the evidentiary documents, specifically the Assignment to MONSANTO COMPANY referenced below, and certifies that to the best of my knowledge and belief, title remains in the name of the Assignee.

Pursuant to MPEP § 324(2), the undersigned avers that he is empowered to sign this statement on behalf of assignee.

ASSIGNEE: MONSANTO COMPANY

Date: January 21, 1999

By:

  
Name: Jon H. Beusen

Registration No. 30,610

Title: Intellectual Property Counsel

ASSIGNMENT:

☒ Enclosed for recording

☐ Previously recorded

Date: \_\_\_\_\_

Reel: \_\_\_\_\_

Frame: \_\_\_\_\_

Jon H. Beusen  
Intellectual Property Counsel  
Authorized to sign this document for  
Monsanto Company by resolution dated  
April 24, 1996 of the Board of Directors

ARNOLD, WHITE & DURKEE

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DECLARATION

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name.

I believe we are the original, first and joint inventors of the subject matter which is claimed and for which a patent is sought on the invention entitled **"POLYMER BLENDS CONTAINING POLYHYDROXYALKANOATES AND COMPOSITIONS WITH GOOD RETENTION OF ELONGATION,"** the Specification of which was filed on **October 27, 1998** as Application Serial No. **09/179,780**.

We hereby state that we have reviewed and understand the contents of the above-identified specification, including the claims.

We acknowledge the duty to disclose to the Patent and Trademark Office all information known to us to be material to patentability of the subject matter claimed in this application, as "materiality" is defined in Title 37, Code of Federal Regulations, § 1.56.

We hereby claim priority benefits under Title 35, United States Code, § 119 of any foreign application(s) for patent, United States provisional application(s), or inventor's certificate listed below and have also identified below any foreign application for patent, United States provisional application, or inventor's certificate having a filing date before that of the application on which priority is claimed:

PRIORITY APPLICATION(S)			Priority Claimed
60/063,852	U.S.A.	October 31, 1997	Yes
(Number)	(Country)	(Date Filed)	Yes/No

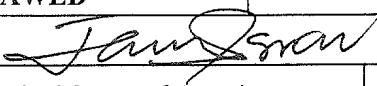
We hereby claim the benefit under Title 35, United States Code, § 120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, § 112, we acknowledge the duty to disclose all information known to us to be material to patentability of the subject matter claimed in this application, as "materiality" is defined in Title 37, Code of Federal Regulations, § 1.56, which become available between the filing date of the prior application and the national or PCT international filing date of this application: **NONE**.

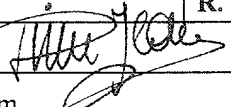
We hereby direct that all correspondence and telephone calls be addressed to:

**Vikki Meriwether, Paralegal**  
**ARNOLD, WHITE & DURKEE**  
**P. O. Box 4433**  
**Houston, Texas 77210-4433**  
**(713) 787-1400**

WE HEREBY DECLARE THAT ALL STATEMENTS MADE OF OUR OWN KNOWLEDGE ARE TRUE AND THAT ALL STATEMENTS MADE ON INFORMATION AND BELIEF ARE BELIEVED TO BE TRUE; AND FURTHER THAT THESE

STATEMENTS WERE MADE WITH THE KNOWLEDGE THAT WILLFUL FALSE STATEMENTS AND THE LIKE SO MADE ARE PUNISHABLE BY FINE OR IMPRISONMENT, OR BOTH, UNDER SECTION 1001 OF TITLE 18 OF THE UNITED STATES CODE AND THAT SUCH WILLFUL FALSE STATEMENTS MAY JEOPARDIZE THE VALIDITY OF THE APPLICATION OR ANY PATENT ISSUED THEREON.

Inventor's Full Name:	JAWED	ASRAR
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Inventor's Full Name:	JEAN	R.	PIERRE
Inventor's Signature:			
Country of Citizenship:	Belgium	Date: 12/17/98	
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